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An Innovative Method for the Evaluation of Particle Deposition Accounting for Rotor/Stator Interaction

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Solid particle ingestion is one of the principal degradation mechanisms in the compressor and turbine sections of gas turbines. In particular, in industrial applications, the microparticles not captured by the air filtration system can cause deposits on blading and, consequently, result in a decrease in the compressor performance. This paper presents three-dimensional numerical simulations of the microparticle ingestion (0.15–1.50 μm) in a transonic axial compressor stage, carried out by means of a commercial computational fluid dynamic code. Particles of this size can follow the main air flow with relatively little slip, while being impacted by the flow turbulence. It is of great interest to the industry to determine which zones of the compressor blades are impacted by these small particles. Particle trajectory simulations use a stochastic Lagrangian tracking method that solves the equations of motion separately from the continuous phase. A particular computational strategy is adopted in order to take into account the presence of two subsequent annular cascades (rotor and stator) in the case of particle ingestion. The proposed strategy allows the evaluation of particle deposition in an axial compressor stage, thanks to its capability of accounting for rotor/stator interaction. NASA Stage 37 is used as a case study for the numerical investigation. The compressor stage numerical model and the discrete phase model are set up and validated against the experimental and numerical data available in the literature. The blade zones affected by the particle impact and the kinematic characteristics of the impact of micrometric and submicrometric particles with the blade surface are shown. Both blade zones affected by the particle impact and deposition are analyzed. The particle deposition is established by using the quantity called sticking probability, adopted from the literature. The sticking probability links the kinematic characteristics of particle impact on the blade with fouling phenomenon. The results show that microparticles tend to follow the flow by impacting at full span with a higher impact concentration on the pressure side of rotor blade and stator vane. Both the rotor blade and stator vane suction side are only affected by the impact of smaller particles (up to 1 μm). Particular fluid dynamic phenomena, such as separation, shock waves, and tip leakage vortex, strongly influence the impact location of the particles. The kinematic analysis shows a high tendency of particle adhesion on the suction side of the rotor blade, especially for particles with a diameter equal to 0.15 μm . [DOI: 10.1115/1.4034968]

23 Introduction

24 Each manufacturer's gas turbine has its own tolerances and
25 design constraints, each use its own operational requirements and
26 each installation site its own particular climatic conditions. In any
27 case, in each location gas turbines are involved in performance
28 degradation.

29 Fouling represents a degradation which is generally recoverable
30 with cleaning/washing operations. Therefore, axial compressor
31 fouling is a serious operating problem, and its control is of critical
32 importance for operators of gas turbine-driven power plants, com-
33 pressor stations, and pump stations.

34 The fouling mechanism involves three specific aspects: (i) the
35 environmental conditions (airborne contaminant, salt, etc.) in
36 which the gas turbine operates, (ii) the power plant design and
37 management (filtration system, washing operations, etc.), and (iii)
38 compressor characteristics (pressure ratio, number of stages, etc.).
39 These aspects work together determining the fouling mechanism.
40 For industrial gas turbines, highly effective filtration systems exist
41 [1]. Depending on the type of filtration system used, smaller

particles ($<2 \mu\text{m}$) can enter the engine. These smaller particles are
too small to cause erosion, but they do cause compressor fouling.
Evaluations of fouled compressors have revealed contamination
both on the pressure side and the suction side of the compressor
blades [2].

In order to carry out a comprehensive analysis of the fouling
issue, both numerical studies and experimental approaches should
consider the sticking capability of particles. Theoretically, zones
with a high number of impacts will be more affected by the foul-
ing phenomenon but, in practice, fouling depends only on the
sticking characteristic of particles. The particle sticking on the
blade surface results in an increase of the thickness of the airfoil
and of the surface roughness. Both these events change the flow-
path inside the blade passages, causing (i) an increment of the
boundary layer thickness, (ii) a decrement of the flow passage
area, and (iii) modifications of the 3D fluid dynamic phenomena.

Particle adhesion on the blade surface is a complex phenom-
enon that includes many aspects: (i) the material of the body in
contact, (ii) the surface conditions, (iii) the particle size, (iv) the
impact velocity, and (v) the impact angle. In this paper, the
authors present a numerical study for the ultra-fine powder inges-
tion by a transonic axial compressor stage. This work is the devel-
opment of the analyses reported in Refs. [3] and [4], in which the
CFD simulation is applied to a rotor cascade only for defining

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66 which blade areas are more affected by the particle impact and
67 adhesion. In this paper, the particle ingestion and the subsequent
68 particle deposition on the entire stage are studied by using CFD
69 simulations and a postprocess computational strategy, which
70 allows the rotor/stator interaction to be considered. The main
71 phases of this work are summarized below:

- 72 • validation of the numerical model of the compressor stage by
means of performance curves available in the literature;
- 73 • simulation of the ingestion of a fine powder characterized by
74 three different particle diameters ($0.15\ \mu\text{m}$, $0.50\ \mu\text{m}$, and
75 $1.50\ \mu\text{m}$). The simulation of particle ingestion is performed
separately for the rotor and the stator cascades;
- 76 • determination of the kinematic characteristics (velocity and
77 angle) of particles that impact on the rotor blade and stator
vane according to pressure side and suction side subdivision;
- 78 • estimation of the sticking probability for each particle that
79 impacts the rotor blade and stator vane in order to define the
80 preferable deposition zones as a function of the particle
diameter;
- 81 • application of a postprocess strategy for considering the
82 effect exerted by the rotor blade on the deposition zone loca-
tion of the stator vane surface.

83 Literature Review

84 The results of fouling detection in single or multistage compres-
85 sors have been featured in the literature since 1950s [5]. A thor-
86 ough literature review of experimental studies with regard to the
87 deposition on axial compressor blade surfaces is reported in Refs.
88 [3], [4], and [6]. Tarabrin et al. [7] highlight that the deposit
89 amount is greater on the stator vanes than on the rotor blades due
90 to the cleaning effects provided by the centrifugal forces on dirt
91 particles. Centrifugal force effects also characterize the results
92 obtained by Syverud et al. [8]. The tests show that the salt deposits
93 are mainly found along the leading edge of the first four stages
94 and on the pressure side of the stator vanes along the hub. The salt
95 deposits are generated by salt particles ($<2\ \mu\text{m}$) carried by water
96 droplets and, for this reason, significantly less deposit is observed
97 on the rotor blades compared to the stator vanes.

98 The question that still requires research is the mechanism
99 through which particles reach the suction surface. Particles that
100 deviate from the streamlines will readily impact on the pressure
101 side of the blades, but the mechanism that can deposit particles on
102 the suction side of the blade is not fully understood. Starting from
103 these considerations, the possibilities for investigating particle
104 kinematics are linked to: (i) the abilities to use numerical simula-
105 tions and/or experimental tests for studying the fouling phenom-
106 enon and (ii) the knowledge of how particles are able to stick to
107 blade surface.

108 Numerical simulations of particle behavior in axial compressor
109 cascades can be found in Refs. [3], [4], and [6]. The authors ana-
110 lyze the microparticle trajectories in a transonic [3,4] and in a sub-
111 sonic [6] rotor, in order to discover which blade zones are affected
112 by particle impact and adhesion. In order to numerically investi-
113 gate particle ingestion in an axial compressor stage, particles must
114 be tracked in both the rotating frame of the rotor domain and the
115 stationary frame of the stator domain, passing through an interface
116 which couples the rotor and the stator cascades. In a recent work,
117 Zagnoli et al. [9] report a review of the computational studies per-
118 formed in past years tracking different types of particles through
119 compressor and turbine stages. In these works, most of which deal
120 with erosion in compressors [10,11] and turbines [12–14], and
121 steady (mixing plane and frozen rotor) and unsteady models are
122 employed at the interface between rotating and stationary domains
123 for the rotor/stator coupling. The authors in Ref. [9] study deposi-
124 tion in the first stage of a high-pressure turbine using both steady
125 mixing plane and unsteady sliding mesh calculations, in order to
126 observe differences due to particle size ($3\text{--}15\ \mu\text{m}$) and computa-
127 tional methods. Steady methods are found to over-predict impacts

and deposits relative to unsteady methods by averaging out dis- 128
crete unsteady vane wake motion, which causes particle motion 129
toward blade surfaces. 130

Methodology 131

The methodology adopted here for analyzing particle ingestion 132
in an axial compressor stage is different from that reported in the 133
literature [9–14]. In this case, in fact, particles are not tracked 134
through the interface between rotating and stationary domains, but 135
the analysis is carried out by means of separate particle injections 136
for the isolated rotor and stator cascades. 137

The flow field within the entire compressor stage is initially 138
simulated, with the stage operating at the best efficiency point at 139
the rotor design rotational speed. The coupling between the rotor 140
and the stator is obtained through a mixing plane interface, model- 141
ing a single passage per cascade. 142

After this preliminary calculation, the flow field is solved for 143
the isolated rotor and stator. The flow simulation setup for the 144
rotor and the stator is performed by using the same boundary con- 145
dition types considered for the stage simulation. Radial profiles of 146
flow variables calculated in the stage simulation are exported at 147
the level of the mixing plane interfaces and imposed at the inflow 148
and outflow boundaries of the isolated rotor and the stator, respec- 149
tively. Then, the CFD solver is run for the two cascades separa- 150
tely. In this way, the flow conditions within the individually 151
simulated rotor and stator match those resulting from the entire 152
stage simulation. 153

Particle injections for the isolated rotor and stator take place on 154
the previously solved flow field. Particles are released at the same 155
local velocities as the air flow from an inlet radial plane with 156
equally spaced injection points for both the rotor and the stator. 157
The uniform distribution of injection points allows the realization 158
of a uniform particle injection from the inlet section of each cas- 159
cade. Moreover, since the number of rotor blades is different from 160
that of stator vanes and only a single passage per cascade is mode- 161
led, rotor and stator domains are characterized by different pitch 162
angles. For these reasons, the total number of injected particles is 163
different for the two cascades. 164

The study of particle impact and adhesion on the rotor blade 165
and stator vane is carried out by subdividing the flow channel of 166
the individual cascades into 11 annular stream tubes of the same 167
radial extent. In this way, 11 radial bands of equal width are iden- 168
tified at the inlet and outlet sections of each cascade, and the rotor 169
blade and stator vane are divided along the spanwise direction 170
into 11 strips. In accordance with a uniform particle injection, the 171
number of particles injected from each inlet radial band depends 172
on the band area only and increases from the inner to the outer 173
band, since the band area increases. 174

For the isolated rotor and stator, the location and the kinematic 175
characteristics of particle impact on the blade surface are deter- 176
mined. These data are then used to estimate the sticking probabili- 177
ty of particles that impact on the rotor blade and stator vane, 178
allowing for the definition of the preferable deposition zones. 179

Finally, the results of the isolated rotor and stator characteriza- 180
tions are postprocessed in order to take into consideration the 181
effect of the interaction between the rotor blade and the particles 182
while analyzing deposition on the stator vane. The adopted post- 183
process computational strategy is based on the following 184
assumptions: 185

- the number of particles that stick to the rotor blade (i.e., par- 186
ticles characterized by a sticking probability greater than 0.5) 187
is negligible with respect to the total number of injected partic- 188
les. This approximation is justified by the data reported in 189
Table 1. The particles uniformly injected from the rotor inlet 190
section are thus simply redistributed by the cascade internal 191
flow;
- the particles released from each radial band of the stator inlet 192
section can deposit exclusively on the corresponding strip of

Table 1 Injected and stuck particles for the isolated rotor

d_p (μm)	0.15	0.50	1.50
Injected particles	3,031,305	2,963,849	3,029,539
Stuck particles	45,710	52,402	97,634

193 the stator vane. This implies that the entirety of particle radial
194 motions within the individual annular stream tube is such
195 that particles cannot pass to an adjacent stream tube. This
196 hypothesis is considered acceptable, since the analysis is per-
197 formed at the stage best efficiency point, where no significant
198 radial flows occur, as shown in Fig. 1.

199 On the basis of the previous assumptions, a linear relationship
200 between the number of particles injected from each band of the
201 stator inlet section and the number of particles adhering to the sta-
202 tor vane corresponding strip is assumed. Therefore, the effect of
203 the rotor presence is considered as a magnification/reduction of
204 the adhesions of particles leaving the stator inlet section from
205 each band, according to the particle radial distribution obtained at
206 the rotor outlet section. This strategy is schematically illustrated
207 in Fig. 2.

208 Stage Numerical Model and Validation

209 In order to investigate the microparticle ingestion and adhesion
210 in an axial compressor stage, the NASA Stage 37 is used as the
211 case study geometry. The stage geometry and performance data
212 are gathered from Ref. [15].

213 **Reference Numerical Compressor Stage.** The NASA Stage
214 37 consists of a rotor and a stator. The rotor is composed of 36
215 blades, and the tip clearance at design speed is 0.356 mm (0.45%
216 of the blade span). The stator is composed of 46 vanes, and the
217 hub clearance is not present. To reduce the computational effort,
218 only a single passage per cascade is modeled, as can be seen in
219 Fig. 3.

220 **Numerical Grid.** The grid used in the calculations is a hexahe-
221 dral grid with a total number of 2,201,776 elements. The grid is
222 realized by employing an O-grid around both rotor blade and sta-
223 tor vane surfaces, with local refinements near the hub and shroud
224 regions. The meshes on the rotor blade and stator vane surfaces
225 are shown in Figs. 3(b) and 3(c), respectively. The first grid points
226 on the rotor blade and stator vane surfaces and end walls are posi-
227 tioned in such a way that the y^+ values range from 5 to 100.

228 In the tip region, the grid is split along the center of the rotor
229 blade thickness, and the nodes do not match across the two halves.
230 Here, the mesh is connected using a nonconformal interface. The
231 rotor tip clearance is resolved with four nodes across the gap span.

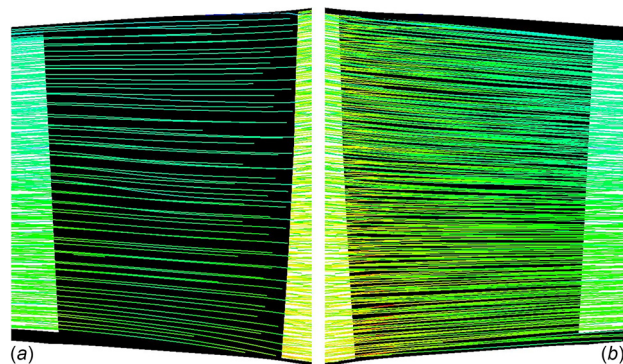


Fig. 1 Streamline pattern within the isolated stator: (a) pres-
sure side and (b) suction side

Numerical Code. The numerical simulations are carried out by
232 means of the commercial CFD code ANSYS Fluent 15.0 [16].
233 The code solves the 3D Reynolds-averaged form of the
234 Navier–Stokes equations by using a finite-volume method. The
235 density-based solver with the implicit solution formulation and
236 Roe-FDS convective flux type is used. For gradient discretization,
237 the Green-Gauss node-based method is selected. A second-order
238 upwind discretization scheme is adopted for flow equations.
239

Turbulence Model. The turbulence model used in the calcula-
240 tions is the standard k - ϵ model, and near-wall effects are modeled
241 by means of standard wall functions. A first-order upwind discreti-
242 zation scheme is selected for both turbulent kinetic energy and
243 turbulent dissipation rate equations.
244

Rotor/Stator Interaction Model. All the compressor stage
245 simulations are performed in a steady multiple reference frame in
246 order to take into account the contemporary presence of moving
247 and stationary domains. A mixing plane model is imposed at the
248 interface between rotating and stationary domains, each of which
249 is solved as a steady-state problem with its own inlet and outlet
250 boundary conditions. The mixing plane interface, whose geometry
251 is radial, is composed by the coupling of an upstream rotor outlet
252 boundary with a downstream stator inlet boundary. The flow-field
253 data at the mixing plane interface are averaged in the circumferen-
254 tial direction on both rotor outlet and stator inlet boundaries. In
255 particular, the mixed-out averaging method provided by the
256 ANSYS Fluent is chosen. The mixed-out average is based on the
257 conservation of mass, momentum and energy, and it is therefore
258 considered a better representation of the flow since it reflects
259 losses associated with nonuniformities in the flow profiles. By per-
260 forming circumferential averages of flow properties at rotor outlet
261 and stator inlet boundaries, profiles of flow variables are defined
262 as a function of the radial coordinate. Radial profiles computed at
263 the rotor outlet are used to update boundary conditions at the sta-
264 tor inlet and vice versa during the calculation process.
265

The computational domain consists of four fluid domains: three
266 stationary domains (inlet duct, stator and outlet duct) and one
267 rotating domain (rotor). Each domain is coupled with the adjacent
268 one through a mixing plane interface. Passing radial profiles of
269 flow variables from adjacent domains in the manner described
270 above requires specific boundary condition types to be defined at
271 the mixing plane interface. All the stage simulations are carried
272 out by assigning pressure outlet and pressure inlet boundary con-
273 dition types to the upstream and downstream sides of each mixing
274 plane interface, respectively. Swirl and total enthalpy conserva-
275 tion is also enforced across the mixing plane interfaces.
276

Properties and Boundary Conditions. An ideal gas approxi-
277 mation is used for air. It is also assumed that the fluid has a con-
278 stant specific heat, thermal conductivity and viscosity.
279

The total pressure, total temperature, and flow direction are
280 assigned to the inflow boundary of the inlet duct. The inlet total
281 pressure $p_{0,1}$ and total temperature $T_{0,1}$ are set equal to 101,325 Pa
282 and 288.15 K, respectively. The flow is defined to be normal at the
283 inflow boundary. Turbulence parameters are specified at the inlet
284 section in terms of turbulence intensity and turbulent viscosity
285 ratio, which are set equal to 5% and 10, respectively.
286

An average relative static pressure $p_{g,3}$ is imposed at the out-
287 flow boundary of the outlet duct, both in the near-choked flow
288 region and in the near-stall region, with radial equilibrium pres-
289 sure distribution. The outflow pressure is progressively increased
290 in order to reproduce the entire performance trend.
291

Rotor blade and stator vane surfaces and end walls are modeled
292 as no-slip, smooth, and adiabatic walls. All the simulations refer
293 to the rotor design rotational speed, equal to 17,188 rpm. Further-
294 more, since only a section of the full geometry is modeled, rota-
295 tional conformal periodic boundary conditions are applied to the
296 lateral surfaces of the flow domain.
297

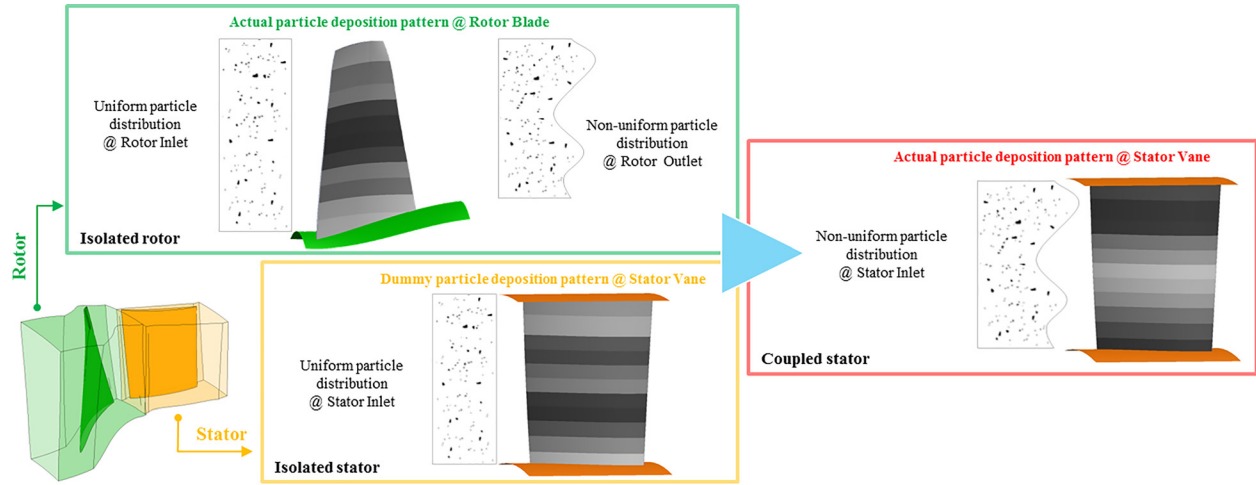


Fig. 2 Schematic illustration of the adopted postprocess computational strategy

298 The results presented in this paper are obtained from conver- 323
 299 gent simulations, with a variation of the residues of the motion 324
 300 and turbulent equations close to zero and all lower than 10^{-4} . 325

301 **Validation.** The validation of the numerical model of the compressor 328
 302 stage is performed by means of comparison with experi- 329
 303 mental measurements gathered from Ref. [15]. This comparison is 330
 304 carried out taking into consideration the total pressure ratio β and 331
 305 the adiabatic efficiency η as a function of the mass flow rate m . 332
 306 The numerical and experimental performance curves are reported 333
 307 in Fig. 4. It can be noticed that the shape of both the experimental 334
 308 performance curves is correctly reproduced by the numerical 335
 309 model. Since the aim of the validation is to obtain a reliable com- 336
 310 pressor stage model, the validation of the numerical model can be 337
 311 considered acceptable. The numerical results are in fairly good 338
 312 agreement with the experimental data. The deviation in terms of 339
 313 mass flow rate at the choked-flow condition is about 3.34%. 340

314 **Particle Model**

315 The solution approach is based on a mathematical model with 341
 316 Eulerian conservation equations for the continuous phase and a 342
 317 Lagrangian frame to simulate a discrete second phase. In this 343
 318 approach, the airflow field is first simulated, and then, the trajec- 344
 319 tories of individual particles are tracked by integrating a force bal- 345
 320 ance equation on the particle. 346

321 **Balance of Forces.** The force balance is comprehensive of 347
 322 inertia, drag, and buoyancy terms. In the force balance, there are 348

two contributes due to the shear stress and diffusion called Saff- 323
 man’s lift force and Brownian force, but these two contributes 324
 become important in very few cases. In this analysis, only the 325
 Brownian term is neglected. An extensive description of the force 326
 balance is reported in Ref. [3]. 327

Near-Wall Particle Behavior. For the particle–wall interac- 328
 tion boundary conditions, a nonadherence condition (named 329
reflect) is imposed on the rotor blade and stator vane surfaces and 330
 end walls. Specific functions and restitution coefficients for the 331
 near-wall particle behavior are implemented by the authors. The 332
 model functions are defined in agreement with Ahlert’s model 333
 [17] and Forder’s coefficients [18]. In a general application, resti- 334
 tution coefficients could depend on (i) impact velocity, (ii) pres- 335
 sure, and (iii) temperature [19]. In this case, only the velocity 336
 could represent an obstacle through the correct representation of 337
 the particle bounce. The restitution coefficients used in this study 338
 are obtained from Forder’s work [18], in which an oilfield control 339
 valve is studied with a flow velocity almost equal to 80 m/s. This 340
 velocity value determines the validity of assuming the restitution 341
 coefficients independent from the velocity. 342

Particle Injection. The particle density ρ_p is set equal to 2560 343
 kg/m^3 , and the variation of the particle diameter d_p is in the range 344
 of 0.15–1.50 μm , while the Stokes number (Eq. (1)), calculated at 345
 the rotor and stator inlet sections, is in the range of 0.0002–0.04 346

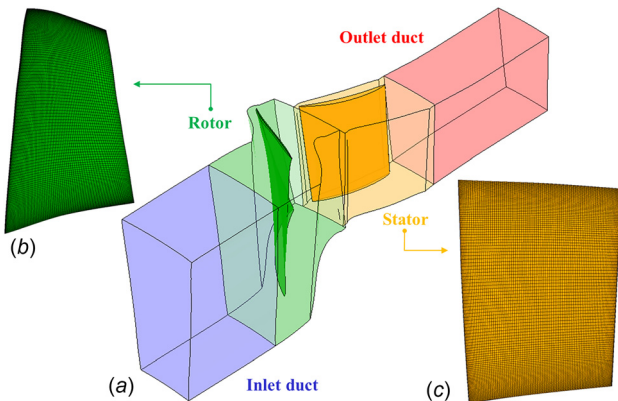


Fig. 3 NASA Stage 37 computational domain: (a) single pas-
 sage model, (b) mesh on rotor blade surface, and (c) mesh on
 stator vane surface

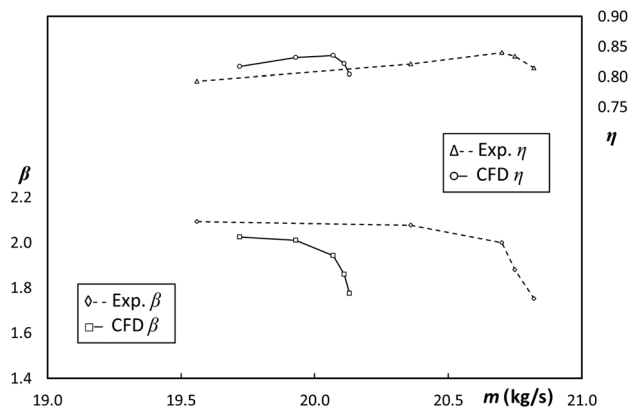


Fig. 4 Comparison between the experimental results (Exp.)
 [15] and CFD results (CFD)

$$St = \frac{\rho_p d_p^2 U_1}{18\mu d_h} \quad (1)$$

348 Particles are spherical and nondeformable. All the analyses refer
349 to injections having particles with the same diameter, the same
350 material, and thus, characterized by the same Stokes number. On
351 the other hand, the total mass flow rate of the discrete phase, m_p ,
352 is linked to the air flow rate and the contaminant concentration.
353 The latter is related to the work environment of the compressor
354 and the efficiency of the filtration system η_f . Since rotor and stator
355 domains are characterized by different pitch angles (and, there-
356 fore, elaborate different air flow rates), a different value of total
357 mass flow rate of contaminants is imposed at the inlet sections of
358 the rotor and the stator. Moreover, it is assumed that particles do
359 not affect the fluid flow (one-way coupling) as the particle's vol-
360 ume fraction is very low ($\ll 10\%$). The injection data for the iso-
361 lated rotor and stator cascades are summarized in Table 1.

362 **Particle Turbulent Dispersion.** The turbulent dispersion of
363 particles in the fluid phase can be predicted by using a stochastic
364 tracking model. The time-averaged flow field determines the
365 mean path of particles, while the instantaneous flow field governs
366 each particle's turbulent dispersion from the mean trajectory. By
367 computing the trajectory in this manner for a sufficient number of
368 particles, the random effects of turbulence on particle dispersion
369 can be included.

370 This investigation uses the discrete random walk (DRW) model
371 to simulate the stochastic velocity fluctuations in the airflow. The
372 DRW model assumes that the fluctuating velocities follow a Gaus-
373 sian probability distribution. This model may give nonphysical
374 results in strongly nonhomogeneous diffusion-dominated flows,
375 where small particles should become uniformly distributed.
376 Instead, the DRW model will show a tendency for such particles
377 to concentrate in low-turbulence regions of the flow. In this case,
378 a specific analysis conducted by the authors shows that the inter-
379 action between the wall, with its boundary layer, and the discrete
380 phase is characterized by the inertial law, as explained in more
381 detail in subsequent paragraphs. For this reason, the diffusion phe-
382 nomena can be neglected and the DRW model can be considered
383 reliable. The number of tracked particles is selected in order to
384 satisfy the statistical independence, since turbulent dispersion is
385 modeled based on a stochastic process.

386 The turbulence model plays a key role in the resolution of particle
387 trajectories near the wall. Through the use of the $k-\varepsilon$ turbu-
388 lence model with standard wall functions there is an isotropic
389 treatment of the turbulence near the wall, and this implies, in the
390 case where the values of y^+ are less than 5, that both the stream-
391 wise mean velocity and the turbulent kinetic energy will be over-
392 estimated [20]. In this study, as mentioned above, the values of y^+
393 do not drop below 5.

394 In Ref. [20], the authors report an extensive sensitivity analysis
395 of the relationship between turbulence models, mesh refinement
396 close to the wall, and particle dimensions expressed by the nondi-
397 mensional particle relaxation time τ^+ , defined as

$$\tau^+ = \frac{(\rho_p/\rho)d_p^2 u_t^2}{18\nu^2} \quad (2)$$

399 where u_t is the shear velocity

$$u_t = \sqrt{\frac{\tau_w}{\rho}} \quad (3)$$

400 and τ_w is the wall shear stress. Tian and Hamadi [20] highlight the
402 effect of a different turbulence model on the velocity deposition
403 for particles in a horizontal and vertical tube. Their study shows
404 that the $k-\varepsilon$ turbulence model with standard wall functions over-
405 predicts the deposition velocity for particles in a *Brownian*

($\tau^+ < 10^{-2}$) and *transition* ($10^{-2} < \tau^+ < 10$) region, and it does
not allow the estimation of the real trend of the particle velocity
deposition. For the *inertial* ($\tau^+ > 10$) region, the $k-\varepsilon$ turbulence
model with standard wall functions over-predicts the deposition
velocity, but in a minor way compared to the other regions, and
the trend of the deposition velocity curve is in agreement with the
other results.

As can be seen in Table 2, the nondimensional particle relaxa-
tion time τ^+ for the simulations presented in this paper is in the
range 2–252, which corresponds to the *transition* and *inertial*
region in accordance with Ref. [20]. For this reason, the $k-\varepsilon$ turbu-
lence model with standard wall functions used for all the analyses
is considered suitable for studying the real deposition phenom-
enon that occurs in the axial compressor stage under investigation.

Isolated Rotor/Stator Characterization

In this paragraph, the results of the characterizations of the iso-
lated rotor and stator cascades are reported. Starting from the anal-
ysis of the kinematic characteristics of particle impact on the
blade surface, the zones characterized by a high probability of par-
ticle deposition are identified by means of the sticking probability
calculation.

Impact Analysis. Only a portion of particles injected from the
inlet section of each cascade impacts on the rotor blade and stator
vane. For comparison among the studied cases, the ratio η_{hit} can
be used. η_{hit} is defined as the ratio between the number of particles
that hit the blade and the total number of injected particles. The
trend of η_{hit} as a function of the particle diameter d_p is shown in
Fig. 5. It is possible to observe that the percentage of particles that
hit the blade surface increases with the particle diameter for both
the rotor and the stator. The number of particles that impact the
rotor blade is very similar to the number of particles that impact
the stator vane, and the two trends are very close to each other. In
Fig. 5, the total number of injected particles and the absolute num-
ber of impacting particles on the blade surface are also reported
for all the studied cases. The results related to the rotor blade
impacts are in line with those presented in the previous work [3].

Regarding the particle impact location on the blade surface,
Fig. 6 shows the trends of the impacting particles on the rotor
blade and the stator vane for all the considered particle diameters:
(i) the η_{hit} values for the pressure side, $\eta_{hit,PS}$, and suction side,
 $\eta_{hit,SS}$, refer to the percentage of particles that hit the pressure side
or suction side compared to the total number of injected particles,
while (ii) the η_{side} values, reported in pie charts, represent the per-
centage of particles that hit the blade on the pressure side or suc-
tion side compared to the total number of particles that hit the
blade.

From the analysis in Fig. 6, it can be seen that by increasing the
particle diameter the number of particles that hit the pressure side
increases in the same manner for the rotor blade and stator vane.
For the suction side, the rotor blade trend decreases as the particle
diameter increases. In the case of the stator vane, the number of
particles that hit the vane with a diameter equal to $1.50 \mu\text{m}$ is
higher than that of particles with a diameter equal to $0.50 \mu\text{m}$. The
differences in the impact trends highlighted for the rotor and stator
are due to the different shape of their airfoils. The stator airfoils
have a thicker leading edge, resulting in a higher capability of col-
lecting particles. These results agree with those presented in Ref.
[6], where a subsonic rotor blade is analyzed. Considering the pie
charts, the results are in line with those reported in the literature in
the case of (i) fouling due to particles with dimensions close to the
unit of micron [2] and (ii) erosion of rotor blades (which involves
larger particles) [11]. In fact, the fouling phenomenon is charac-
terized by a wider distribution of the particles on the blade surface
with respect to erosion, which shows a higher percentage of
impacts on the pressure side than on the suction side. In
Appendix A, an overall representation of the impact zones is

Table 2 Injection data for the isolated rotor and stator

	Rotor			Stator		
d_p (μm)	0.15	0.50	1.50	0.15	0.50	1.50
Stokes number, St	2×10^{-4}	2×10^{-3}	3×10^{-2}	4×10^{-4}	5×10^{-3}	4×10^{-2}
Nondimensional relax. time, τ^+	3	28	252	2	19	167
Filtration eff., η_f (%)	61	65	96	61	65	96
Mass flow rate, m_p (kg/s)	7.3×10^{-7}	2.4×10^{-5}	7.5×10^{-5}	4.3×10^{-7}	1.4×10^{-5}	4.3×10^{-5}

472 illustrated for some representative airfoils for both the rotor blade and the stator vane.
 473 and the stator vane.

474 The modules of the particle impact velocity v_i are reported in
 475 Fig. 7 for the rotor blade and the stator vane. The velocity values
 476 refer to the vector sum of the three velocity components along the
 477 coordinate axes at the impact point on the blade surface. Each dot
 478 is colored by the impact velocity and it is superimposed with
 479 respect to the mesh node that provides the blade shape.

480 For the rotor blade, the effect of the separation that occurs on
 481 the suction side and the impact velocity peaks that take place at
 482 the blade tip area are clearly visible. The shock wave causes the
 483 drop in the particle impact velocity, and at about 50% of the chord
 484 it is possible to find the lowest impact velocity. The stator vane
 485 shows different impact velocity patterns. The impact velocity
 486 peak is located close to the hub in the first part of the airfoil chord
 487 for both the pressure and suction side, while the impact velocity
 488 assumes the lowest values in the vane region close to the shroud,
 489 where a flow separation takes place. The flow separation influen-
 490 ces the particle impact velocity on the suction side near the end
 491 walls. In particular, local three-dimensional phenomena affect the
 492 particle trajectories. Flow separation in the corner region of the
 493 vane passage is common in axial compressors, as reported by
 494 Gbadebo et al. [21]. Moreover, Fig. 7 shows that particle impact
 495 velocities are very different on the same side of the blade. These
 496 differences are due to the shape of the blade (e.g., blade height)
 497 and the fluid dynamic phenomena (e.g., flow separation).

498 The impact velocity is not the only parameter needed to deter-
 499 mine particle adhesion on the blade surface. As mentioned above,
 500 particle adhesion is due to a combination of different effects, but
 501 the most important parameters are the normal v_n and tangential v_t
 502 impact velocity components. Therefore, the particle impact angle
 503 α , which is the angle between the surface normal vector and the

504 impact velocity vector, is analyzed in order to better understand
 505 the kinematic characteristics of particle impact.

506 In Fig. 8, the particle impact angle is reported by means of a
 507 colored particle plot. In some instances the impact angle is greater
 508 than 90 deg. This is due to (i) the surface local curvature (e.g., at
 509 the leading and trailing edges) and (ii) surface reconstruction
 510 approximation during the particle impact postprocess [4,6]. A
 511 deviation can arise from the fact that the surface is reconstructed
 512 by interpolating points on the mesh elements in the vicinity of the
 513 point of impact. The approximation introduced by this procedure
 514 is considered acceptable by the authors, allowing for a confidence
 515 band of ± 5 deg for all the results presented in this paper. Figure 8
 516 illustrates that the impact angle assumes the widest variation at
 517 the leading and trailing edges, due to the surface curvature of the
 518 rotor blade and stator vane. For the pressure side, the rotor blade
 519 shows impact angle values close to 90 deg (i.e., particles are tan-
 520 gential to the blade surface) and, by contrast, the stator vane
 521 shows impact angle values close to 0 deg (i.e., particles are per-
 522 pendicular to the blade surface). The suction side presents almost
 523 the same impact angle values for both the rotor blade and stator
 524 vane, even if, for the rotor blade, the effects of flow separation are
 525 still visible.

526 **Adhesion Analysis.** A quantitative analysis of particle adhe-
 527 sion on the isolated rotor, and stator is provided by using the
 528 experimental results found in Ref. [22], in which particle velocity
 529 and materials are among the most similar to the particles causing
 530 the fouling phenomenon. As the authors in Refs. [4], and [6]
 531 previously showed, starting from the experimental sticking probabili-
 532 ty trends reported in Ref. [22], it is possible to define
 533 representative trends for the correlation between the normal

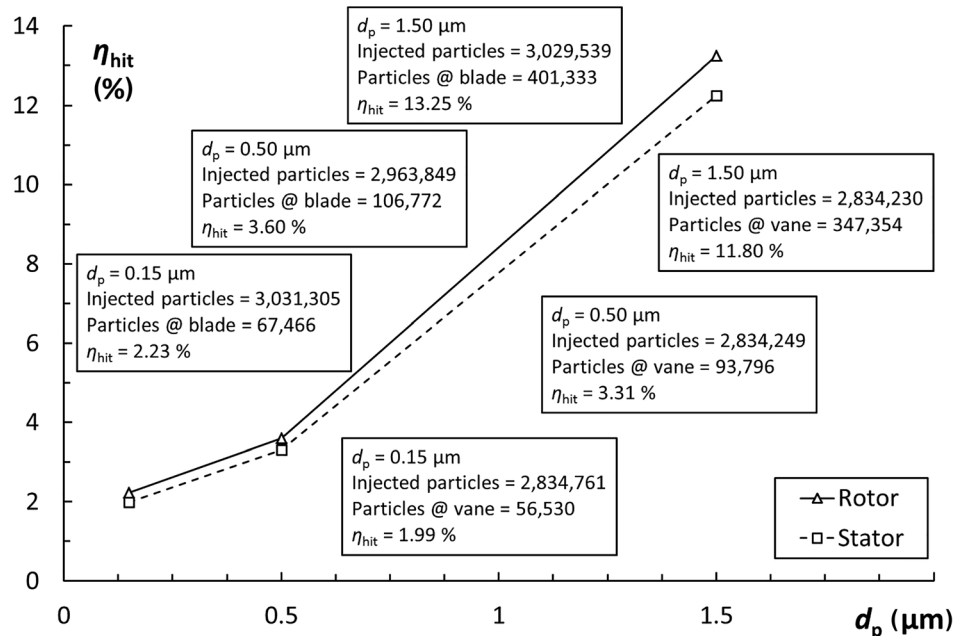


Fig. 5 Capture efficiency versus particle diameter for the isolated rotor and stator

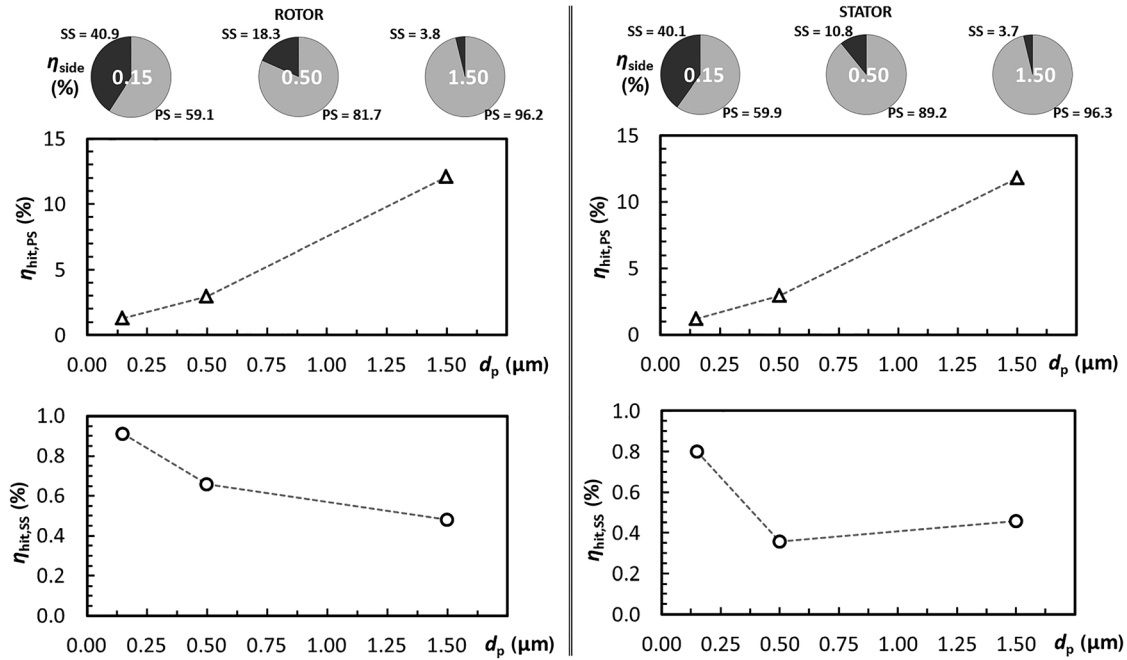


Fig. 6 Particle impact distributions for the isolated rotor and stator

534 impact velocity v_n and the sticking probability SP. The modules
 535 of v_n are shown in Appendix B for the rotor blade and the stator
 536 vane. For particle diameters lower than $0.50 \mu\text{m}$, the equation that
 537 links v_n with SP for lower normal impact velocities ($<4 \text{ m/s}$) is

$$S_p = -0.09v_n + 0.99 \quad (4)$$

539 while for higher impact velocities (4–90 m/s), it is

$$S_p = 2 \times 10^{-6}v_n^3 - 0.000378v_n^2 + 0.011800v_n + 0.587100 \quad (5)$$

540 In the case of particle diameter higher than $0.50 \mu\text{m}$, the equation
 542 for lower normal impact velocities ($<4 \text{ m/s}$) is

$$S_p = -0.112v_n + 0.990 \quad (6)$$

543 while for higher impact velocities (4–90 m/s) it is

$$S_p = -6 \times 10^{-5}v_n^2 - 6e - 4v_n + 0.545 \quad (7)$$

On the basis of the previous relations, for smaller particles the
 545 sticking probability is equal to 0.5 at a normal impact velocity of
 546 48.35 m/s. Instead, for bigger particles the sticking probability is
 547 equal to 0.5 for a normal impact velocity of 22.85 m/s. Therefore,
 548 the smaller particles have a wider range of normal impact velocity
 549 for which particle impact with the blade surface becomes (with a
 550 high probability) a permanent adhesion. Equations (4)–(7) are
 551 used to calculate the sticking probability for each particle that
 552 impacts on the surface by using the normal impact velocity.

Because of the particle-wall interaction settings, particles do
 553 not stick to the surfaces. Particles bounce on the rotor blade, stator
 554 vane, and end walls following the rules imposed by the restitution
 555 coefficients. In the literature, some studies can be found on the
 556 effects of the particle bounce especially related to erosion phe-
 557 nomena [10]. Bouncing particles possess high kinetic energy, that
 558

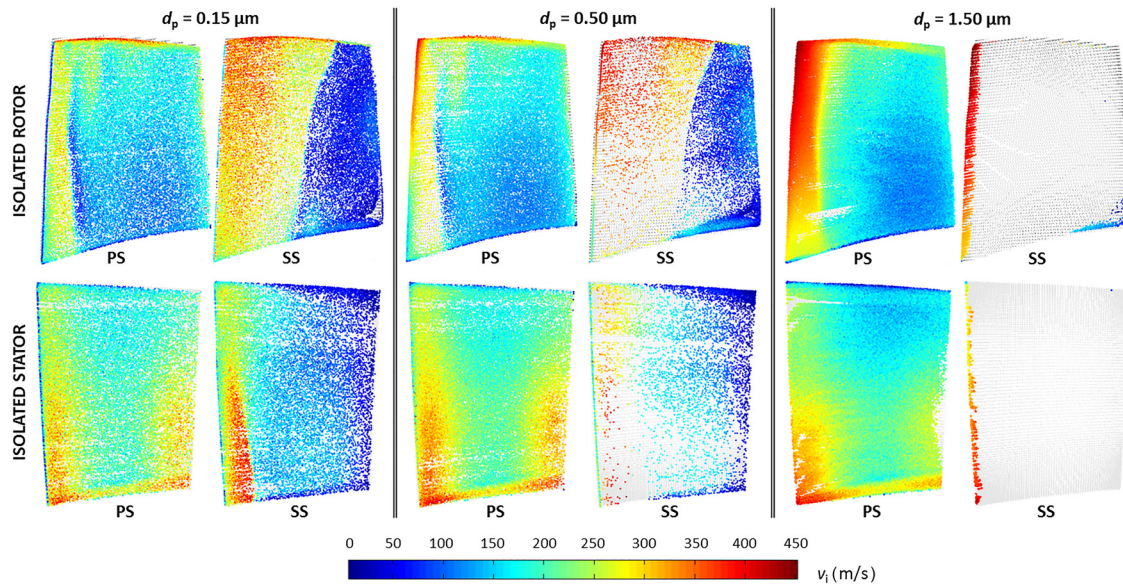


Fig. 7 Particle impact velocity for the isolated rotor and stator

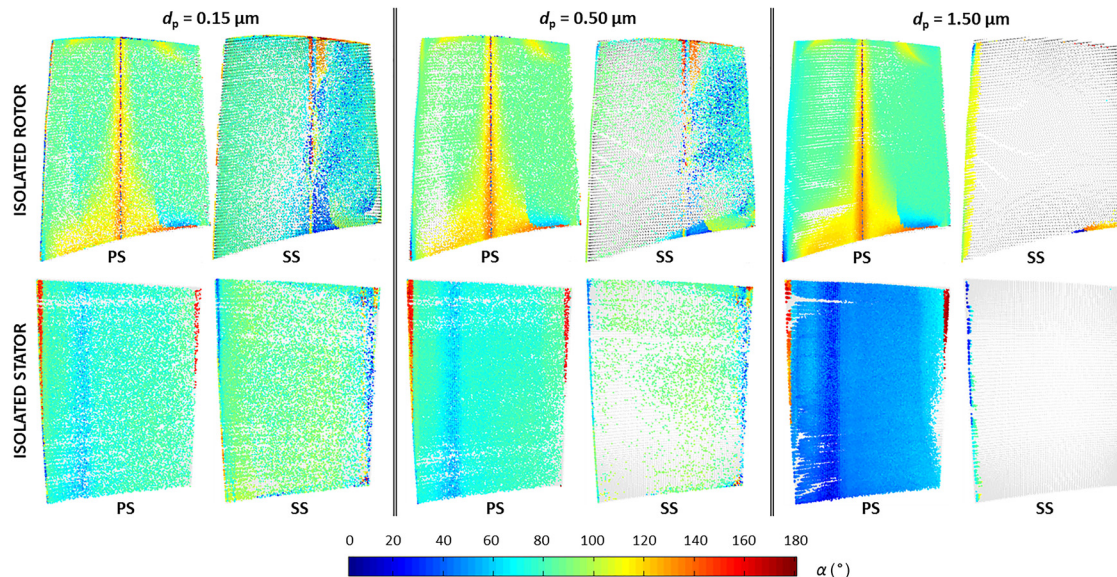


Fig. 8 Particle impact angle for the isolated rotor and stator

559 decreases by an order of magnitude during the first impact [22].
 560 Such a phenomenon implies that these particles will not be able to
 561 stick during the first contact, but, instead, it will most likely be
 562 during the second one. In fact, the decrease in kinetic energy is
 563 related to the decrease in velocity and, consequently, to an
 564 increase in sticking probability. For this reason, the particle adhesion
 565 values take into account the particle bounces. More specifically,
 566 the bounces of each particle are analyzed in terms of normal impact
 567 velocity and only when the normal impact velocity value allows
 568 particle sticking (i.e., the sticking probability is greater than 0.5)
 569 the particle is considered stuck to the surface, and the subsequent
 570 bounces, if present, are erased.

571 In Fig. 9, the trend of the ratio $\eta_{\text{hit,SP}>0.5}$ (black continuous
 572 line) for particles characterized by a sticking probability greater
 573 than 0.5, superimposed with the trend of the ratio η_{hit} (gray dotted
 574 line), is reported. The two trends refer to both sides (pressure and
 575 suction side) of the rotor blade and stator vane. As can be seen,
 576 the trend of $\eta_{\text{hit,PS,SP}>0.5}$ for the pressure side of both the rotor
 577 blade and stator vane does not follow the trend of $\eta_{\text{hit,PS}}$, unlike
 578 the trends of $\eta_{\text{hit,SS,SP}>0.5}$ for the suction side. For the pressure
 579 side, the number of stuck particles is quite independent from the
 580 total number of particles that hit the blade and $\eta_{\text{hit,PS,SP}>0.5}$
 581 remains almost the same for the three considered particle diameters.
 582 In this case, the larger particles produce more fouling effects
 583 due to their greater diameter and thus their greater mass. The two
 584 percentages are very close to each other only for the smallest particles,
 585 showing the high capability of smaller particles to stick to the
 586 blade surface. For the suction side, the trend of the ratio
 587 $\eta_{\text{hit,SS,SP}>0.5}$ highlights a very high percentage of particles able to
 588 stick for the smallest diameters compared to the total number of
 589 particles that hit the suction side. For higher particles, the percentage
 590 is very low due to the very low number of particles that reach
 591 the suction side.

592 The particles that stick to the rotor blade and stator vane are
 593 shown in Fig. 10 by using black dots. Each dot represents a stuck
 594 particle (i.e., a particle for which the sticking probability is greater
 595 than 0.5). Smaller particles are able to cover the entire blade surface
 596 (pressure and suction side), even though a small portion of the
 597 blade close to the leading edge appears free from deposits.
 598 Moving to bigger particles, the suction side and certain zones of
 599 the pressure side are less affected by particle deposition.

600 Fluid dynamic phenomena influence the particle deposition patterns
 601 as illustrated in Ref. [23], where field data regarding the deposition
 602 of foulants on a transonic compressor blade are reported.
 603 The authors show the blade surface condition after 25,000 h of

604 operation and highlight that three-dimensional flow features cause
 605 small particles to be deposited in zones where secondary flows
 606 and vortices are dominant. Figure 11 shows a qualitative comparison
 607 between the actual deposits on a rotor blade taken from Ref. [23]
 608 and the numerical results of the present analysis ($0.50 \mu\text{m}$
 609 particles). Depending on the blade side, it is possible to observe
 610 similar deposition patterns. The effect of the shock wave is clearly
 611 visible on the suction side of the blade, where a narrow region
 612 which is free from deposit can be detected. For the pressure side,
 613 a greater amount of deposits is present in the second part of the
 614 blade chord, especially close to the hub and at blade midspan. At
 615 the leading edge of the blade, a particular deposition pattern can
 616 be seen. The effect of the stagnation determines the high presence
 617 of impacting particles on the leading edge and, by contrast, there
 618 are no particles in the area immediately downstream. This phenomenon
 619 is more evident in the case of smaller particles that impact the
 620 rotor blade, where the velocity field could be characterized by
 621 normal shock waves due to the local curvature of the airfoil [24].
 622 Regarding the stator vane, the latter phenomenon is still
 623 observable and, in this case, the thicker nose of the airfoil determines
 624 the blade capability of collecting particles. Similar results can
 625 be found in Ref. [8]. The deposition on the leading edge represents
 626 a key aspect, because the changes in the leading edge area (shape,
 627 size, and surface roughness) are one of the most important causes
 628 of performance degradation due to fouling [25] and erosion [26].
 629 Deposit distributions, different from the pressure side and suction
 630 side moving to higher particle diameters, agree with those reported
 631 in the literature in the case of (i) fouling due to particles with
 632 dimensions close to the unit of micron [2] and (ii) erosion of rotor
 633 blades (which involves larger particles) [11].

634 In general, the rotor blade and stator vane show almost the same
 635 behavior related to particle sticking, even though the effects on the
 636 stage performance are different. As reported by Morini et al. [27],
 637 the effects of rotor deposits (e.g., surface roughness and airfoil
 638 thickness) on stage performance are greater with respect to those
 639 generated by the same amount of deposits on the stator vane.
 640

641 As described above, the sticking probability defined in Ref. [22]
 642 only considers the normal impact velocity. However, in this applica-
 643 tion particular attention must be paid to the tangential impact
 644 velocity v_t . In fact, as can be seen in Appendix B, the magnitude
 645 of v_t is not negligible. The tangential impact velocity can reach
 646 250 m/s or 400 m/s on the pressure side and suction side, respectively.
 647 These very high velocity values could diminish the sticking probability
 648 and transform an adhesion-impact into a

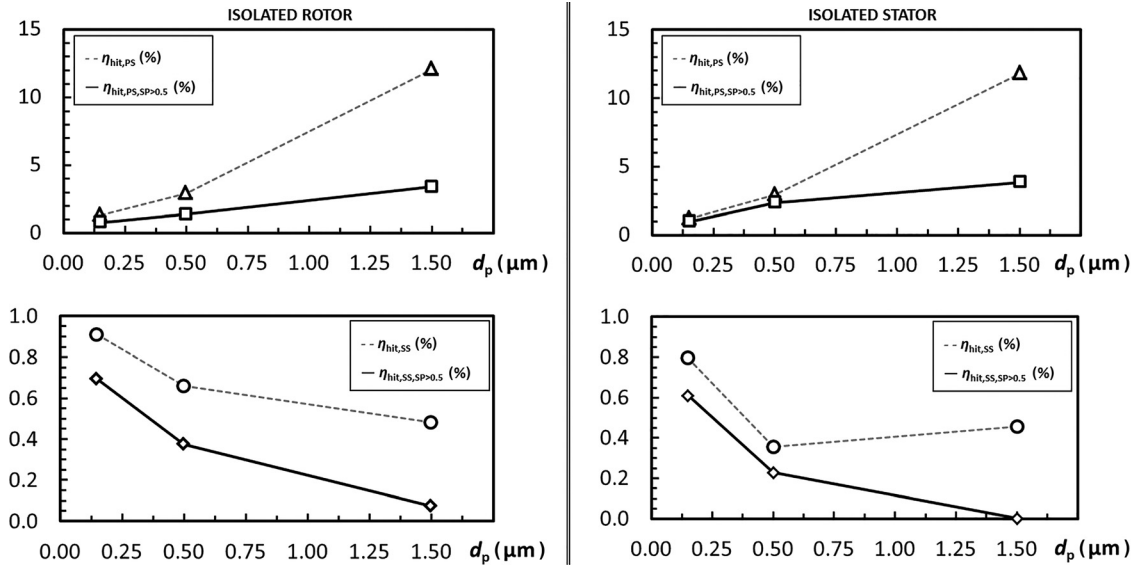


Fig. 9 Trends of the ratio $\eta_{hit,SP>0.5}$ and η_{hit} superimposed for the isolated rotor and stator

649 slip-impact (specific studies on the interaction between normal
 650 and tangential impact velocities are not available in the literature).
 651 Conversely, it can be noted that in the suction side separation
 652 zone of the rotor blade, the tangential impact velocity is much
 653 smaller, thus, limiting the possibility of slip between the particles
 654 and blade surface.

655 **Coupled Stator Analysis**

656 The particle deposition patterns for the stator vane shown in
 657 Fig. 10, which result from the characterization of the isolated stator
 658 cascade, are not representative of the actual deposits, since
 659 they are determined starting from a uniform particle injection.
 660 Actually, the deposits on the stator vane surface are the conse-
 661 quence of the action exerted by the rotor blade on the particle tra-
 662 jectories. In order to consider the effect of the interaction between
 663 the rotor blade and the particles while analyzing deposition on the
 664 stator vane, the postprocess computational strategy previously
 665 described is applied.

666 Figure 12 reports the trends of the ratio $\eta_{hit,SP>0.5}$ for both sides
 667 of the stator vane, in accordance with the spanwise subdivision of
 668 the vane into 11 strips. It is possible to observe the higher

669 capability of particles to stick to the pressure side of the stator
 670 vane. The vane surface appears contaminated in a uniform way,
 671 and the deposits do not afflict a specific area. In general, the
 672 suction side shows a more irregular trend, especially close to the end
 673 wall regions.

674 The localization of the deposits on the blade represents a key
 675 aspect in the fouling phenomenon. In particular, the presence of
 676 the dangerous particles at the top of the blade could be responsible
 677 for a greater drop in compressor performance. As reported by Aldi
 678 et al. [28], the effects of fouling at the blade tip (e.g., the increase
 679 in surface roughness) have a greater influence on compressor per-
 680 formance degradation. The difference in the deposits between the
 681 pressure side and suction side is also important. As pointed out by
 682 Morini et al. in Ref. [29], the effects of fouling on the suction side
 683 (e.g., the increase in surface roughness) have a greater influence
 684 on compressor performance degradation.

685 **Conclusions**

686 In this paper, an extended numerical analysis of microparticle
 687 ingestion and adhesion in a transonic axial compressor stage is
 688 carried out. The NASA Stage 37 is considered the reference

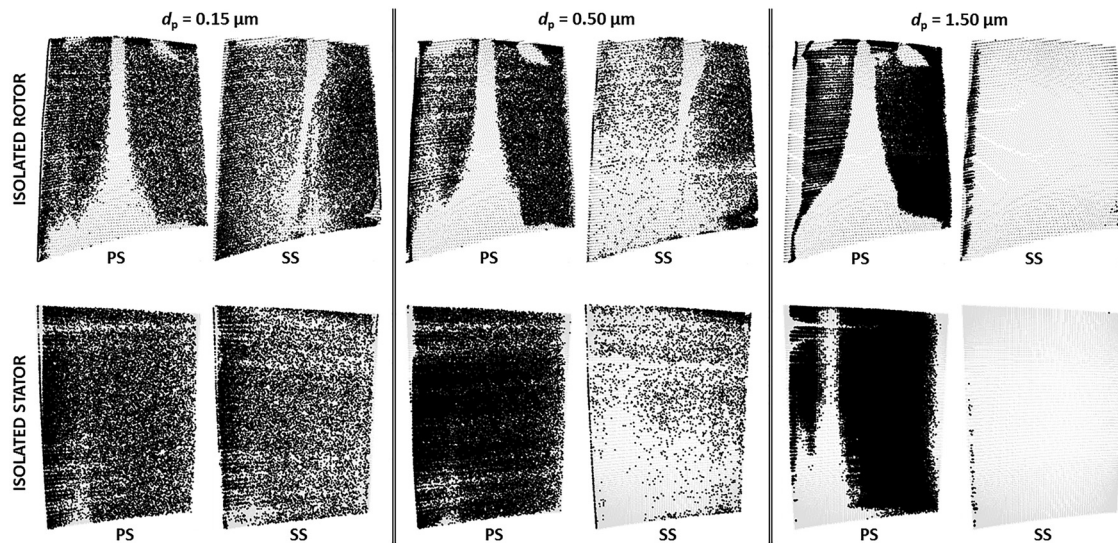


Fig. 10 Particle deposition patterns for the isolated rotor and stator

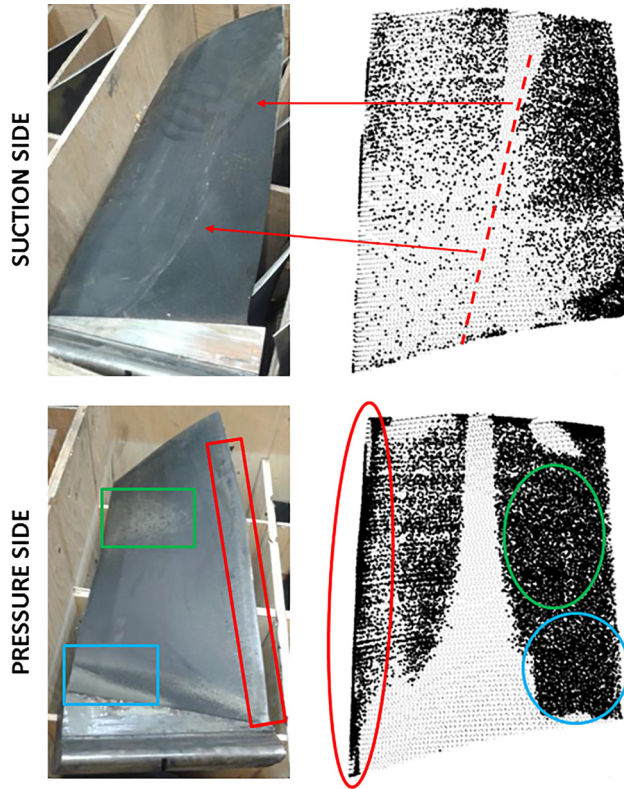


Fig. 11 Qualitative comparison between the actual deposits on the rotor blade [23] and numerical results

689 compressor stage. Numerical simulations are performed by using
 690 realistic field data for air contaminant concentration and filtration
 691 efficiency. Particle trajectories are predicted by means of an
 692 Eulerian–Lagrangian CFD approach, with separate particle injections
 693 for the isolated rotor and stator cascades. The location and
 694 the kinematic characteristics of particle impact on the blade surface
 695 are determined. These data are then used to calculate the sticking
 696 probability of particles that impact on the rotor blade and
 697 stator vane, defining the zones characterized by a high probability
 698 of particle deposition. A postprocess computational strategy is
 699 then used in order to consider the effect exerted by the rotor blade
 700 on the deposition zone location on the stator vane.
 701 The key results obtained in this work can be summarized as follows:
 702 (i) the percentage of particles that hit the rotor blade and stator
 703 vane increases with the diameter of particles and, (ii) by
 704 increasing the particle diameter, the suction side is less affected
 705 by particle impacts than the pressure side. Regarding the kinematic
 706 characteristics of particle impact and its sticking

probability, the following results are obtained: (i) the particle
 impact velocity depends on several factors (surface local curva-
 ture and fluid dynamic phenomena, such as flow separation and
 tip leakage vortex) and (ii) on the suction side, the smallest particles
 are the most numerous from a fouling point of view, due to
 the high total number of particles characterized by a sticking prob-
 ability greater than 0.5. In general, the rotor blade and stator vane
 show almost the same behavior in relation to particle sticking. In
 fact, the suction side is less affected by deposits by increasing the
 particle diameter, and bigger particles stick only to the pressure
 side.

The understanding of fouling mechanisms in compressors is
 still a challenge for manufacturers and users. An increase in the
 knowledge of fouling through the use of numerical codes may
 therefore constitute a decisive element for better planning of tur-
 bomachinery maintenance.

Acknowledgment

The authors would like to thank Devid Dainese MSc for his val-
 uable work in performing the particle postprocess.

Nomenclature

- d = diameter
- m = mass flow rate
- St = Stokes number
- U = averaged velocity
- u_t = shear velocity
- v = velocity
- y^+ = non-dimensional distance

Greek Symbols

- α = impact angle
- β = total pressure ratio
- η = efficiency
- μ = dynamic viscosity
- τ_w = wall shear stress
- τ^+ = nondimensional particle relaxation time
- ν = kinematic viscosity
- ρ = density

Subscripts and superscripts

- f = filtration system
- h = hydraulic
- hit = particle that impact a surface
- i = impact
- n = normal direction
- p = particle
- side = side (referring to the blade and vane side)

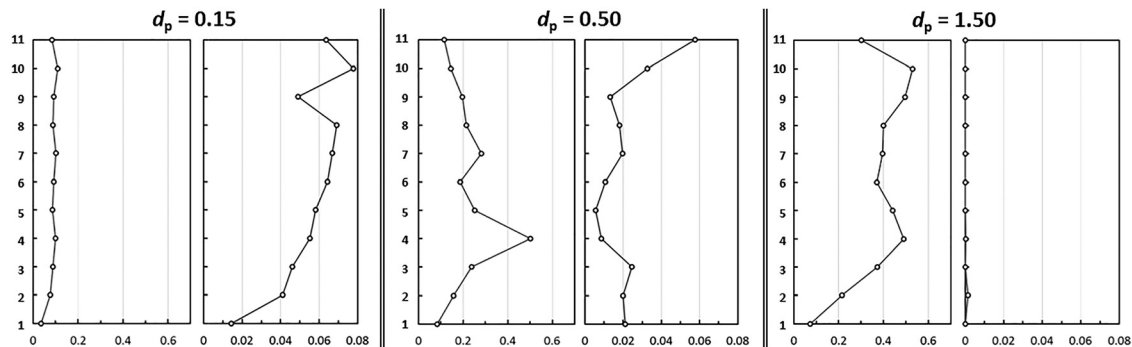


Fig. 12 Trends of the ratio $\eta_{hit,SP>0.5}$ for the coupled stator according to the spanwise subdivision of the stator vane

751 t = tangential direction
 752 1 = inlet section of the stage
 753 3 = outlet section of the stage

754 **Acronyms**

755 CFD = computational fluid dynamics
 756 DRW = discrete random walk
 757 PS = pressure side
 758 SP = sticking probability
 759 SS = suction side

Appendix A

Overall Impact Patterns

760

761

All the particle impact patterns are shown in Fig. 13. Each pattern represents the projection of the fouled airfoil into a perpendicular plane with respect to the spanwise direction. On the left side, the spanwise station and the correspondent percentage of the blade span are reported. The rotor blade and stator vane are divided by 11 strips along the spanwise direction and each dot

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763

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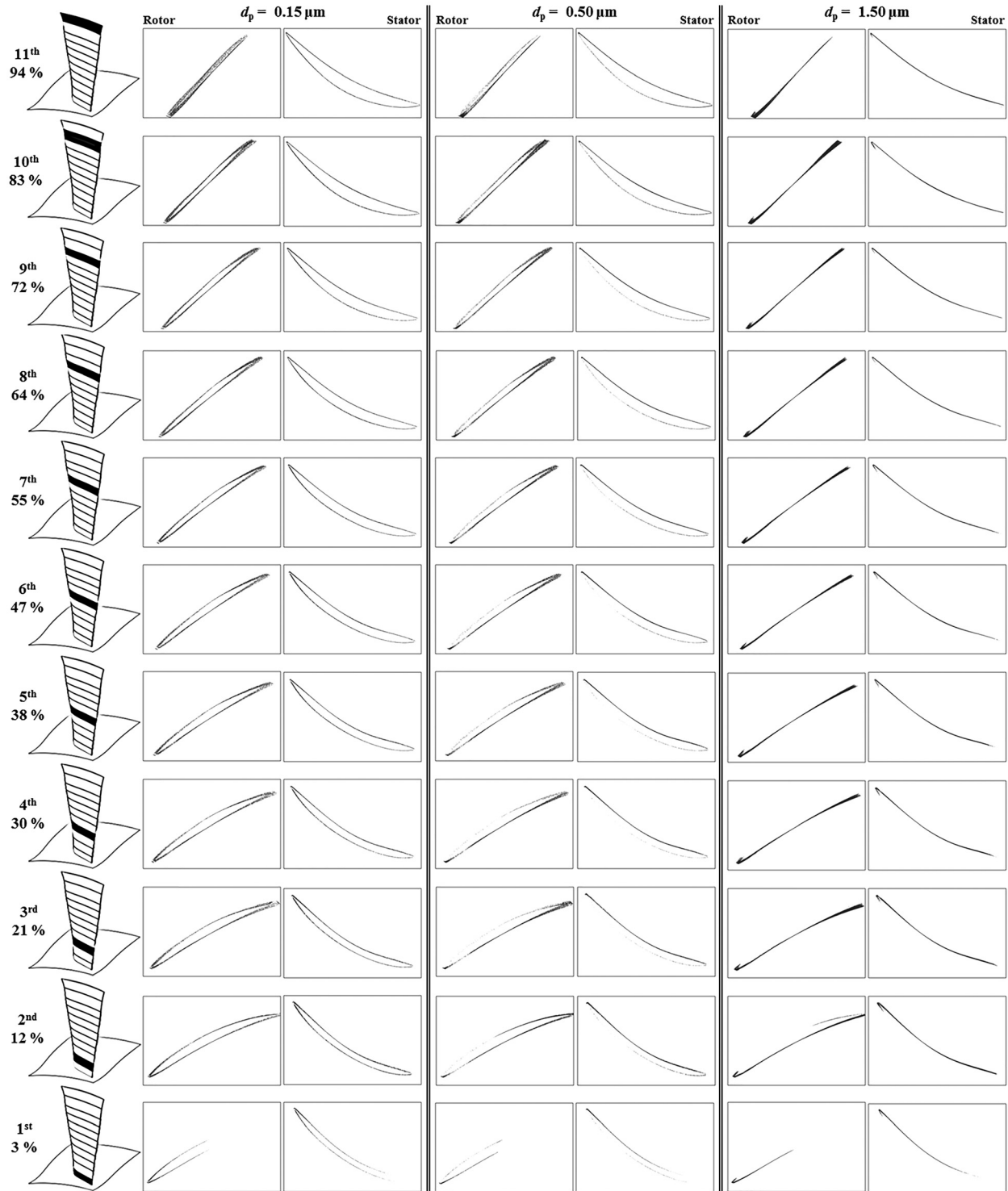


Fig. 13 Spanwise subdivision (left side) and overall impact patterns

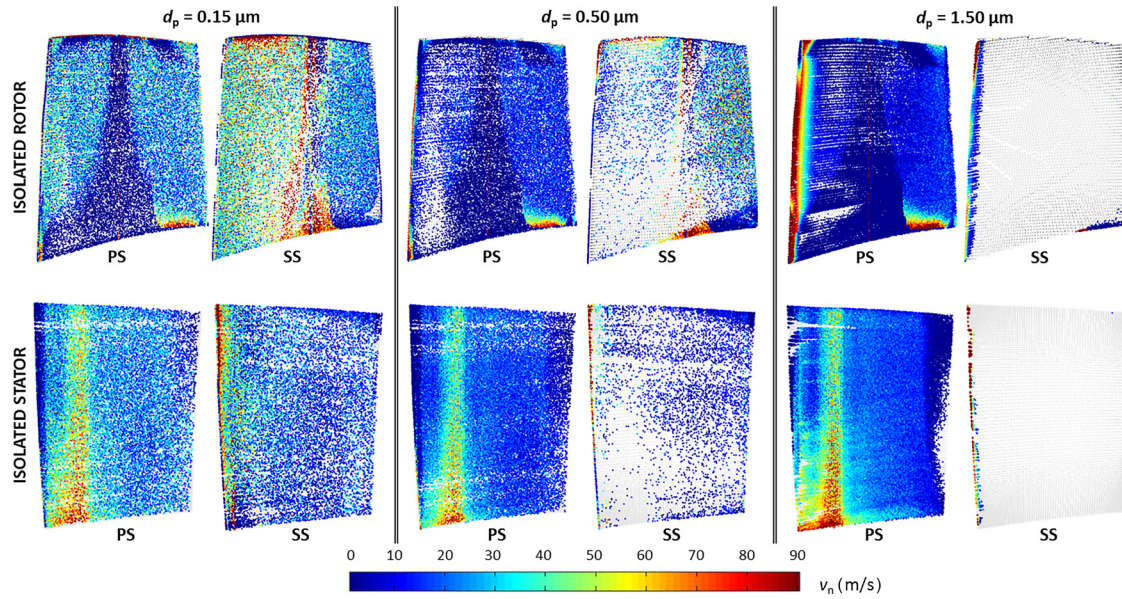


Fig. 14 Particle normal impact velocity for the isolated rotor and stator

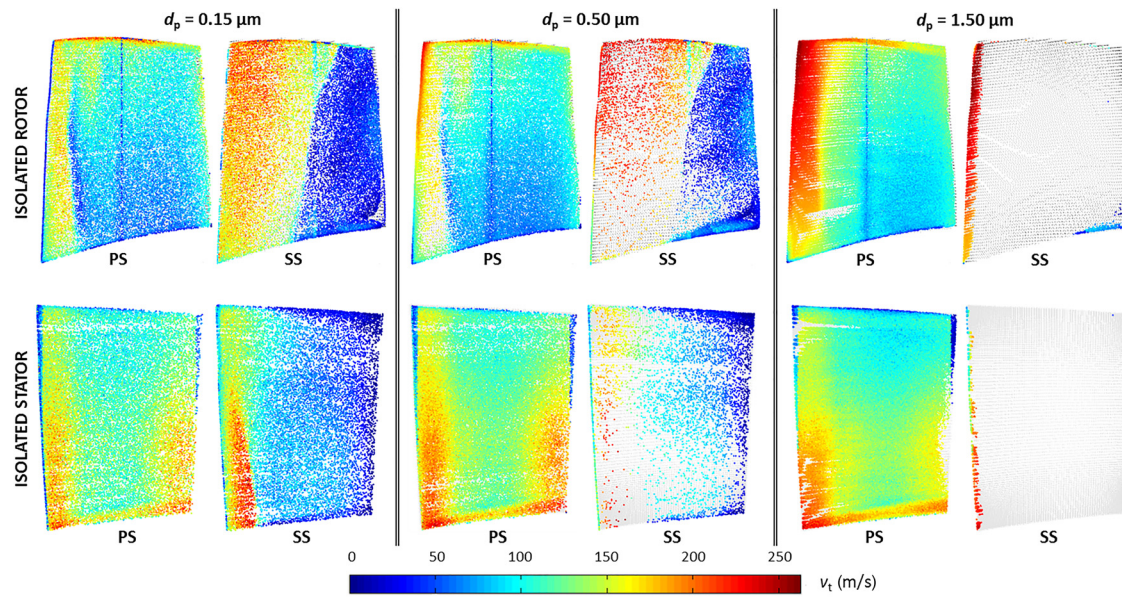


Fig. 15 Particle tangential impact velocity for the isolated rotor and stator

768 represents a single particle that hits the blade. Because of the
 769 shape of the hub, which develops along the streamwise direction
 770 with different diameters, the projection of the rotor blade is not
 771 complete, and only the first half of the airfoil can be represented.

772 **Appendix B**

773 **Normal and Tangential Impact Velocity Components**

774 The modules of the particle normal v_n and tangential v_t impact
 775 velocity components are reported in Figs. 14 and 15, respectively,
 776 for the rotor blade and the stator vane. Each dot is colored by the
 777 normal/tangential impact velocity and is superimposed with
 778 respect to the mesh node that provides the blade shape.

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